ALLOY C-276

ALLOY C-276 (UNS N10276/W.Nr. 2.4819) is known for its corrosion resistance in a wide range of aggressive media. The high molybdenum content imparts resistance to localized corrosion such as pitting. The low carbon minimizes carbide precipitation during welding to maintain resistance to intergranular attack in heat affected zones of welded joints. It is used in chemical processing, pollution control, pulp and paper production, industrial and municipal waste treatment and the recovery of "sour" natural gas. Applications in air pollution control include stack liners, ducts, dampers, scrubbers, stack-gas re-heaters, fans and fan housings. In chemical processing, the alloy is used for components including heat exchangers, reaction vessels, evaporators and transfer piping.

Corrosion Resistance

ALLOY C-276 is resistant to general corrosion, stress corrosion cracking, pitting and crevice corrosion in a broad range of severe environments. Its resistance to carbide precipitation during welding maintains corrosion resistance in the heat affected zones of welded joints. It has exceptional resistance to sulfuric acid and hydrochloric acid. It resists many of the most severe media encountered in chemical processing, including reducing and oxidizing acids, highly oxidizing, neutral, and acid chlorides, solvents, formic and acetic acids, acetic anhydride, wet chlorine gas, hypochlorites, and chlorine solutions. It has excellent resistance to phosphoric acid. At all temperatures below the boiling point and at concentrations lower than 65 wt %, tests have shown corrosion rates of less than 5 mpy (0.13 mm/y). ALLOY C-276 exhibits excellent resistance to corrosion by seawater especially under crevice conditions which induce attack in other commonly used materials such as 316 stainless steel, ALLOY 400, and ALLOY 625.

The performance of ALLOY C-276 in a severe test for susceptibility to intergranular attack (ASTM G 28) is shown below in Table 8. The base corrosion rates listed are representative of typical production material. Rates significantly higher than these indicate susceptibility to intergranular attack. This test is designed to verify mill production only and not to compare alloys for use in applications such as flue gas desulfurization.

Corrosion Resistance Flue Gas Desulfurization

ALLOY C-276 is useful for flue gas desulfurization (FGD) systems to control air pollution from electric power plants. The alloy is used for various applications including scrubbers, ducting and stack liners.

Scrubber liquors and gas condensates generally contain chlorides and the chloride level often determines the corrosion behaviour of the materials.

ALLOY C-276 has been shown to withstand higher chloride content than other alloys before the onset of localized corrosion in a simulated scrubber environment.

Corrosion Resistance Oilfield Applications

ALLOY C-276 is one of the premier materials for recovery and handling of "sour" natural gas, which contains hydrogen sulfide and usually carbon dioxide and chlorides. The gas can be extremely corrosive to carbon and alloy steels, and may cause brittle failure of many alloys by sulfide stress cracking (hydrogen embrittlement) or stress corrosion cracking. The high levels of nickel, chromium, and molybdenum in ALLOY C-276 make the alloy resistant to sour environments even at high temperatures in deep wells. The alloy is used for tubing and a variety of other downhole and surface components.

Heat Treatments

Hot forming should be between 1600 and 2250°F (870 and 1230°C), with all heavy forming above 2000°F (1090°C). ALLOY C-276 is normally annealed at 2100-2150°F (1150-1175°C) and rapidly cooled such as by water quenching.

Welding

ALLOY C-276 has good weldability and can be used as welded for most applications.

Table 1 - Limiting Chemical Composition, %

Nickel	
Molybdenum	15.0-17.0
Chromium	14.5-16.5
Iron	4.0-7.0
Tungsten	3.0-4.5
Cobalt	2.5 max.
Manganese	1.0 max.
Carbon	0.01 max.
Vanadium	0.35 max.
Phosphorus	0.04 max.
Sulfur	0.03 max.
Silicon	0.08 max.

Table 3 - Physical Constants

Density, lb/in ³	0.321
g/cm ³	8.89
Melting Range, °F	2415-2500
°C	1325-1370
Thermal Conductivity, Btu•in/ft²•h•°F	67.9
W/m•°C	9.8
Specific Heat, Btu•lb•°F	0.102
J/kg•°C	427
Young's Modulus, 10 ³ ksi	29.8
GPa	205
Shear Modulus, 10 ³ ksi	11.4
GPa	79
Permeability at 200 oersted (15.9 kA/m)	1.0002
Poisson's Ratio	0.307

Table 2 - Physical Properties

Temp	Thermal Conductivity	Coeff. of Expansion ^a	Electrical Resistivity	Young's Modulus	
°F	Btuein./ft2eh°F	10 ⁻⁶ in/in•°F	ohm•cmil/ft	10 ³ ksi	
-270	50	-	-	141	
-100	60	1.F.	0		
0	65	-	1 5		
77	-	878	739.2	29.8	
100	71	-	-		
200	77	6.8	743.8	29.5	
400	90	7.0	749.3	28.6	
600	104	7.2	757.7	27.8	
800	117	7.4	760.3	26.7	
1000	132	7.5	772.5	25.7	
1200	145	7.7	781.5	24.8	
1400	159	8.1	773.9	23.5	
1600	173	8.5	768.3	22.0	
1800	185		766.2	20.6	
2000	195	=	757.7	19.1	
°C	W/m•°C	μm/m•°C	μΩ•cm	GPa	
-168	7.2	-	170	- 24	
-73	8.7	1570	:74	. 	
20	9.8	14	-	-	
25	u u	(T)	122.9	205	
100	11.2	12.2	123.7	203	
200	12.8	12.4	124.5	198	
300	14.7	12.9	125.7	192	
400	0 16.4 13.2		126.0	186	
500	18.2	13.5	127.7	180	
600	20.0	13.6	129.9	178	
700	21.9	14.1	129.7	167	
800	23.7	14.8	128.2	159	
900	25.4	-	127.4	150	
1000	27.0		127.1	141	
1100	28.3	37.	-		

^aMean coefficient of linear expansion between 77°F (25°C) and temperature shown.

Table 4 - Elevated Temperature Dynamic Modulus Properties

Temperature	Young's Modulus	Shear Modulus	Poisson's	
°F	10 ³ ksi	10 ³ ksi	Ratio	
70	31.30	11.81	0.33	
100	31.18	11.75	0.33	
200	30.77	11.57	0.33	
300	30.35	11.40	0.33	
400	29.92	11.23	0.33	
500	29.42	11.05	0.33	

Table 5 - Corrosion Rates in Acid Solutions^a

Temperature		erature	Corrosion Rate, mpy (mm/a)				
Solution	°F	°C	alloy C-276	alloy 22	alloy 625	alloy 686	
10% H ₂ SO ₄	Boiling	Boiling	20 (0.51)	22 (0.56)	17 (0.43)	3 (0.08)	
20% H ₂ SO ₄	176	80	3 (0.08)	1 (0.03)	1 (0.03)	-	
40% H ₂ SO ₄	176	80	5 (0.13)	10 (0.25)	5 (0.13)	74	
80% H ₂ SO ₄	176	80	4 (0.10)	9 (0.23)	6 (0.15)	4 (0.10)	
95% H ₂ SO ₄	122	50	0.1 (0.003)	-	48 (1.2)	-	
5% H ₂ SO ₄ + 0.1% HCl	Boiling	Boiling	22 (0.56)	24 (0.61)	-	-	
10% H ₂ SO ₄ + 1% HCl	Boiling	Boiling	70 (1.78)	201 (5.11)	465 (11.68)	-	
10% H ₂ SO ₄ + 2% HCl	Boiling	Boiling	138 (3.51)	281 (7.14)	-	132 (3.35)	
10% H ₂ SO ₄ + 2% HCl	122	50	0.2 (0.005)	0.1 (0.003)	0.1 (0.003)	0 (0)	
10% H ₂ SO ₄ + 5% HCl	Boiling	Boiling	256 (6.50)	456 (11.58)	-	-	
40% H ₂ SO ₄ + 10% HCl	176	80	26 (0.66)	32 (0.81)	-	-	
2% HCI	Boiling	Boiling	43 (1.09)	52 (1.32)	-	6 (0.15)	
5% HCI	140	60	10 (0.25)	-	46 (1.17)	1.2 (0.30)	
20% HCI	212	100	154 (3.91)	269 (6.83)	385 (9.78)	-	
5% HCl + 2% HF	158	70	18 (0.46)	40 (1.02)	102 (2.59)	-	
85% H ₃ PO ₄	Boiling	Boiling	10 (0.25)	13 (0.33)	>180 (>4.57)	16 (0.41)	
10% HNO ₃ + 3% HF	Boiling	Boiling	95 (2.41)	23 (0.61)	28 (0.71)	-	

a168 h tests.

Table 6 - Corrosion Rates in Hydrochloric, Phosphoric and Acetic Acids^a

	Temperature		Corrosion Rate, mpy (mm/a)					
Solution	°F	°C	alloy C-276	alloy 25-6MO	alloy 27-7MO	alloy 22	alloy 686	
0.2% HCI	Boiling	Boiling	0.60 (0.02)	<0.1 (<0.003)	1.3 (0.03)	<0.1 (<0.003)	0.20 (0.005)	
1% HCI	Boiling	Boiling	6.5 (0.17)	119 (3.02)	<0.1 (<0.003)	2.7 (0.07)	2.0 (0.05)	
	194	90	3.5 (0.09)	37.0 (0.94)	<0.1 (<0.003)	-	~	
	158	70	0.74 (0.02)	0.02 (<0.001)	<0.1 (<0.003)	=:	=	
5% HCI	158	70	13.2 (0.34)	142 (3.61)	150 (3.8)	18.8 (0.48)	9.8 (0.25)	
	122	50	0.5 (0.01)	43.4 (1.10)	5 (0.13)	1 (0.03)	0 (0)	
85% H ₃ PO ₄	Boiling	Boiling	10.4 (0.26)	114 (2.90)	27 (0.69)	13.0 (0.33)	16.2 (0.41)	
	194	90	0.20 (0.005)	10.6 (0.27)	<0.1 (<0.003)	0.21 (0.005)	0.18 (0.005)	
80% CH ₃ COOH	Boiling	Boiling	0.15 (0.004)	<0.1 (<0.003)	<1 (<0.03)	<0.1 (<0.003)	<0.1 (<0.003)	

a192 h tests.

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Table 8 - ASTM G28 Tests for Intergranular Attack

Method A^a

Corrosion Rate

mm/a

4.45

Method B^b

Corrosion Rate

mm/a

0.76

mpy

30

Table 7 - Corrosion Rates in Various Media^a

Temperature Corrosion Rate Solution °F °C mpy mm/a 15^b 10% HNO₃ 0.38b Boiling Boiling 10% HNO₃ + 2% HCl 180 82 6.5 0.17 15% HNO₃ + 3% HF 140 60 179 4.55 20% HNO₃ + 2% HF 140 215 60 5.46 3% HF 176 80 53 1.35 10% HF 75 24 2 0.05 10% HF 176 80 28 0.71 75 Concentrated HF 24 1 0.03 Concentrated HF 176 80 34 0.86 20% H₃PO₄ Boiling Boiling < 0.03 <1 60% H₃PO₄ Boiling Boiling 1 0.03 85% H₃PO₄ 212 100 <1 < 0.03 85% H₃PO₄ Boiling 10 Boiling 0.25 99.9% CH₃COOH Boiling Boiling <1 < 0.03 + 0.1% NaCl 50% NaOH Boiling Boiling 0.03 1 10% HBr 176 80 <1 < 0.03 10% HBr Boiling Boiling <1 < 0.03 10% NH₃Br 176 0.00 80 0 Boiling 10% NH₃Br Boiling 0 0.00

Alloy

alloy C-276

mpy

175

Table 9 - Critical Crevice and Critical Pitting Temperatures in an Acidified 6% Ferric Chloride Solution (ASTM G 48, Methods C & D)

Alloy		Crevice erature	Critical Pitting Temperature		
,,	°C	°F	°C	°F	
alloy 686	>85	>185	>85	>185	
alloy 22	75	167	>85	>185	
alloy C-276	50	122	>85	>185	
alloy 27-7MO	45	122	>85	>185	
alloy 625	35	95	>85	>185	
alloy 25-6MO	35	86	70	158	
alloy 825	5	41	30	86	
AISI Stainless Steel	<0	<32	20	68	

Table 10 - Corrosion Rates^a in Simulated FGD Mixed-Gas Condensate Solutions

Solution	Tempe	erature	Corrosi	on Rate, mp	y (mm/a)
	°F	°C	alloy C-276	alloy 22	alloy 625
Solution 1 ^b	185	85	82 (2.08)	20 (0.51)	14 (0.36)
Solution 2°	176	80	42 (1.07)	50 (1.27)	126 (3.20)

a168 h test.

^aBoiling ferric sulfate/50% sulfuric acid.

^bBoiling 23% H₂SO₄ + 1.2% HCl + 1% FeCl₃ + 1% CuCl₂.

^aTest duration of 168 h except as noted.

^bTest duration of 24 h.

^b60% H₂SO₄ + 0.5% HCl + 0.1% HF + 0.1% HNO₃.

 $^{^{}c}60\% \text{ H}_{2}\text{SO}_{4} + 2.5\% \text{ HCl} + 0.2\% \text{ HF} + 0.5\% \text{ fly ash.}$

Table 11 - Maximum Pitting or Crevice Attack, mils (mm), in FGD Scrubber Slurry^a

Alloy	Quencher	Absorber	Absorber Outlet	Outlet Duct	Bypass Duct
AISI 316L	22 (0.56)	21 (0.53)	35 (0.89) ^b	35 (0.89) ^b	12 (0.30)
AISI 317LM	20 (0.51)	22 (0.56)	29 (0.74)	33 (0.84)	29 (0.74)
alloy 825	15 (0.38)	33 (0.84)	39 (0.99)	50 (1.27) ^b	10 (0.25)
alloy 625	<2 (<0.05)	10 (0.25)	11 (0.28)	7 (0.18)	nil
alloy C-276	nil	nil	<2 (<0.05)	nil	nil

^a6-month exposure at 126°F (52°C), pH 5.5, 5000 ppm chlorides.

Table 12 - Maximum Pitting or Crevice Attack, mils (mm), in Scrubber Slurry^a

Alloy	Scrubber Bottom	Under Spray Nozzles	Scrubber Outlet	Hold Tank
AISI 316	5 (0.13)	7 (0.18)	49 (1.24) ^b	2 (0.05)
alloy 825	<2 (<0.05)	1.2 (0.03)	49 (1.24) ^b	nil
alloy 625	nil	nil	26 (0.66)	nil
alloy C-276	nil	nil	nil	nil

^a3-month exposure at 120°F (49°C), pH 5.8-6.1, 10,000 ppm chlorides.

Table 13 - C-Ring Tests in NACE Solution^a

Material Condition	Simulated Well Age	Yield Strength (0.2% Offset)		9		Hardness,	Duration,	Sulfide Stress
		ksi	MPa	Rockwell C Days		Cracking		
Cold Worked	600°F (315°C)/1000 h	126.6	873	32	43	No		
Cold Worked	600°F (315°C)/1000 h	155.1	1069	38	43	No		
Cold Worked	600°F (315°C)/1000 h	166.8	1150	35	43	No		
Cold Worked	600°F (315°C)/1000 h	188.7	1301	43	43	No		

aRoom-temperature tests at 100% of yield strength in 5% NaCl plus 0.5% acetic acid saturated with H₂S. All specimens were coupled to carbon steel.

^bPerforated.

^bPerforated.

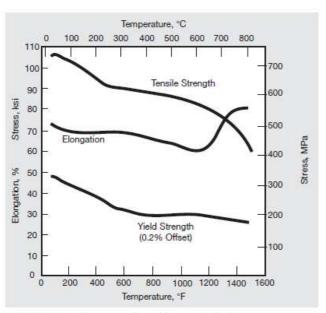


Figure 1. Tensile properties of annealed plate.

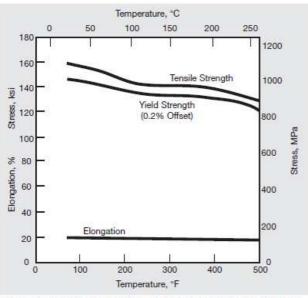


Figure 3. Tensile properties of 33.5% cold-worked tubing.

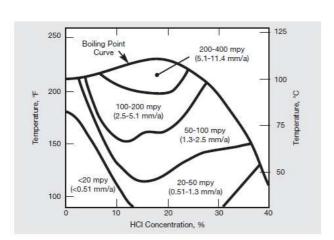


Figure 5. Corrosion rates in oxygen-saturated hydrochloric acid.

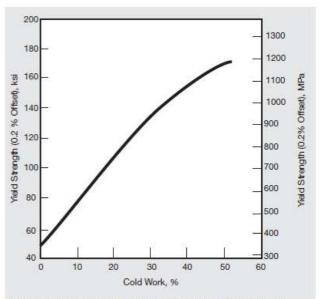


Figure 2. Effect of cold work on the yield strength of annealed plate.

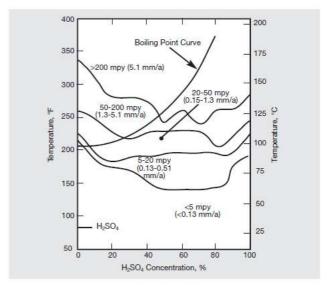


Figure 4. Corrosion rates in sulfuric acid.

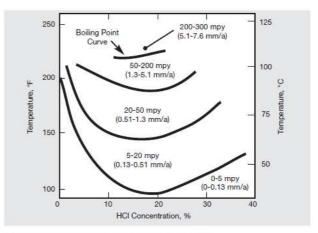


Figure 6. Corrosion rates in hydrochloric acid.

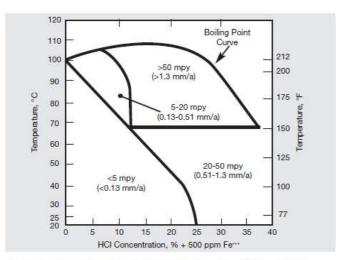


Figure 7. Corrosion rates in hydrochloric acid + 500 ppm Fe***

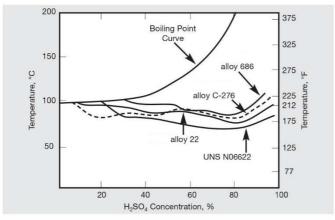


Figure 9. Comparative behavior of several nickel base alloys in sulfuric acid. The isocorrosion curves show temperatures and concentrations above which the corrosion rate exceeds 0.5 mm/a (20 mpy).

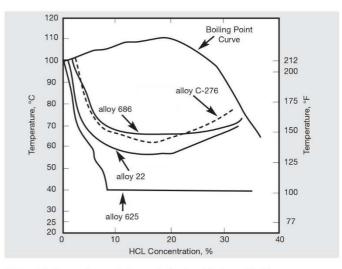


Figure 8. Corrosion resistance in hydrochloric acid. The isocorrosion curves show temperatures and concentrations above which the corrosion rate exceeds 0.5 mm/a (20 mpy).

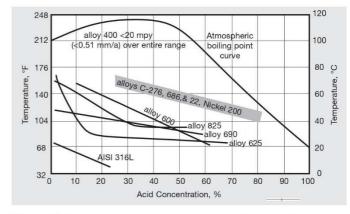


Figure 10. A summary iso-corrosion chart for 20 mpy (0.51 mm/a) data in hydrofluoric acid.